

Supporting Information

for

Rapid gas-liquid reaction in flow. Continuous synthesis and production of cyclohexene oxide

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Beilstein J. Org. Chem. 2022, 18, 660-668. doi:10.3762/bjoc.18.67

Experimental and analytical data

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General

GC-MS analysis was performed on SHIMADZU GCMS-QP2020NX using a fused silica capillary column (Agilent, HP-PONA; $0.20~\text{mm} \times 50~\text{m}$; initial oven temperature, 40~°C). ^1H and ^{13}C NMR spectra were recorded on a JEOL JNM-ECZ400S (^1H 400 MHz, ^{13}C 100 MHz) spectrometer with Me₄Si or CDCl₃ as a standard in CDCl₃ unless otherwise noted. Cyclohexene, isobutyraldehyde, and tridecane were purchased from Tokyo Chemical Industry Co., Ltd. and used without further purification. 1,2-dichloroethane was purchased from Fujifilm Wako Pure Chemical Corporation and used without further purification. The air cylinder was purchased from Medical Sakai

Stainless steel (SUS316) microtube reactors with inner diameter of 1.00 and 2.17 mm were purchased from GL Sciences and were cut or connected into appropriate lengths The micromixer and microtube reactors were connected with stainless steel fittings (GL Sciences) to construct the flow microreactor in the laboratory. The flow microreactor was dipped in an oil bath to control the temperature. Solutions were continuously introduced to the flow microreactor using a plunger pump, DFC FC-F-PP-110S.

Experimental.

General procedure for epoxidation of cyclohexene with air bubbling in batch reactors

The same procedure as described in the literature was followed [1]. In a 100 ml two-necked flask equipped with a cooling condenser through which -15 °C cooling solvent was circulated, a solution of isobutyraldehyde (9.75 mmol) and tridecane as an internal standard in 1,2-dichloroethane (45 mL) was stirred vigorously with air bubbling at reaction temperature for 30 min. Then, a solution of cyclohexene (3.25 mmol) in 1,2-dichloroethane (5 mL) was added. Inner pressure was released from a thin needle on the top of the condenser. The reaction temperature was controlled either in a water bath or an oil bath. At a certain reaction time, 50 μ L of the reaction solution was taken out using a gastight syringe and immediately diluted with deuterated chloroform for 1 H NMR analysis to determine the conversion of cyclohexene and yield of cyclohexene oxide.

General procedure for epoxidation of cyclohexene with air in flow reactors

A flow microreactor system consisting of a T-shaped micromixer and one microtube reactor was used for the epoxidation of cyclohexene with air. A solution of cyclohexene (0.065 M), isobutyraldehyde (3 equivalents, 0.195 M), and tridecane as an internal standard in 1,2-dichloroethane (flow rate: 2.6 ml/min) exposed to Ar flow was introduced into a mixer by a plunger pump. Air was introduced into a mixer at the flow rate of 480 ml/min. The resulting mixture was passed through the microtube reactor ($\phi = 2.17$ mm, L = 20 m, residence time = 1.4 min) which was immersed in an oil bath. The resulting solution was collected in a vessel for 1 min, then a small amount of it was immediately diluted with deuterated chloroform and analyzed by ¹H NMR to obtain the conversion of cyclohexene and yield of cyclohexene oxide.

Data table

Table S1. Yield of cyclohexene oxide in the epoxidation of cyclohexene with air bubbling in batch at various temperatures.

	reaction time (min)					
temperature	30	60	120	180	270	570
40 °C	11%	15%	17%	19%	_	-
60 °C	32%	42%	62%%	72%	75%	74%
80 °C	17%	24%	30	41%	-	_

Yield of cyclohexene oxide was determined by ¹H NMR analysis.

Table S2. Investigation of the reaction temperature in flow epoxidation of cyclohexene at a residence time of 0.35 min.

temperature (°C)	conversion (%) ^a	yield (%) ^a	yield/conversion (%)
40	19	0	
60	28	1	5
80	41	12	28
100	73	47	64
120	90	47	52

^a Determined by ¹H NMR analysis.

Table S3. Investigation of residence time in flow epoxidation of cyclohexene at 100 °C.

residence time (min)	conversion (%) ^a	yield (%) ^a	
0.14	43	26	
0.35	73	47	
0.7	90	70	
1.4	98	84	
2	100	46	

^a Determined by ¹H NMR analysis.

Table S4. Continuous production of cyclohexene oxide

duration time (min)	conversion (%) ^a	yield (%) ^a	integrated productivity (g/h) ^b
0-5	100	94	0.3
5-10	100	91	0.6
10-15	100	94	0.9
15-20	100	91	1.2
20-25	100	93	1.5
25-30	100	92	1.8
30-35	100	93	2.1
35-40	100	91	2.4
40-45	100	92	2.8
45-50	100	91	3.1
50-55	100	93	3.4
55-60	100	94	3.7

^a Determined by ¹H NMR analysis. ^b Calculated based on theoretical productivity for 5 min operation and yield of cyclohexene oxide.

Table S5. Effect of concentration of cyclohexene and equivalent of aldehyde.

concentration of	ratio of cyclohexene and aldehyde		productivity
cyclohexene (M) ^a	(cyclohexene : aldehyde)	yield (%) ^b	(g/h) ^c
0.065	1:3	84	0.8
0.26	1.3	93	3.3
0.26		97	3.9
0.52	1:2	95	7.6
0.78		93	11.1

^a Solution in 1,2-dichloroethane with isobutyraldehyde and tridecane. ^b Determined by ¹H NMR analysis. ^c Calculated based on theoretical productivity and yield of cyclohexene oxide.

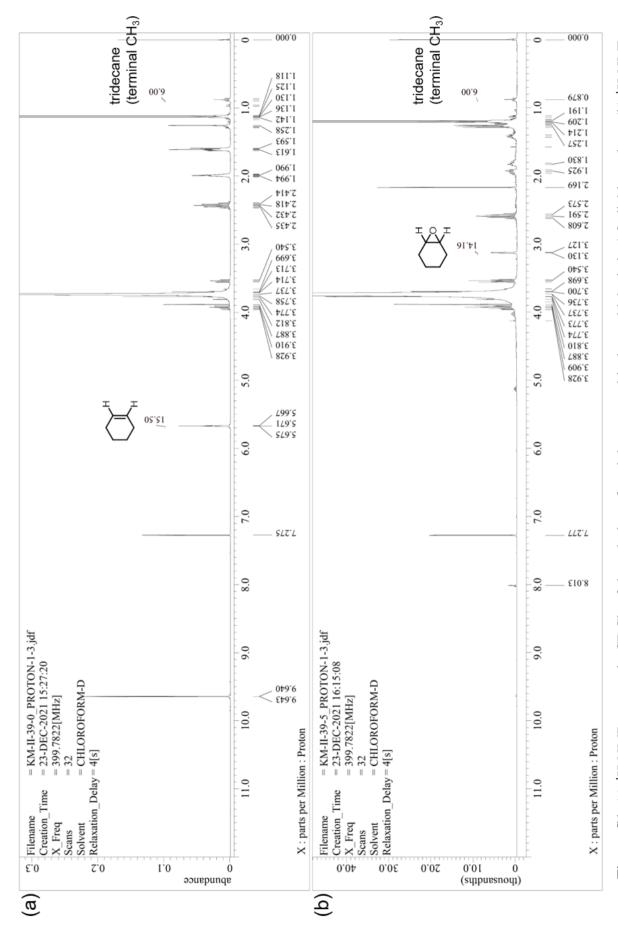


Figure S1. (a) ¹H NMR spectra in CDCl₃ of the solution of cyclohexene and isobutyraldehyde in 1,2-dichloroethane (b) ¹H NMR spectra in CDCl₃ of the eluted solution collected in the 1-hour continuous flow experiment (>99% conv, 91% yield)

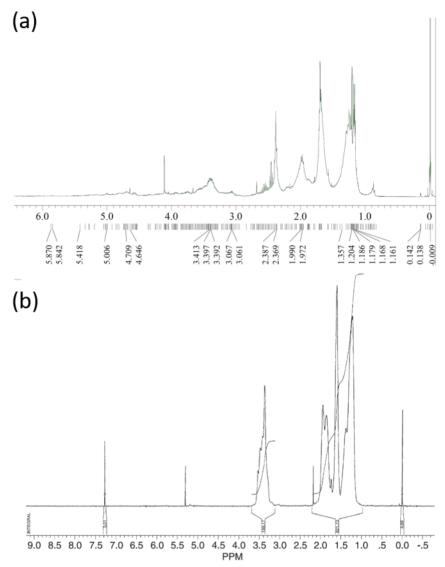


Fig. 10. ¹H NMR (400 MHz) spectrum of poly (cyclohexene oxide) in CDCl₃.

Figure S2. (a) ¹H NMR spectra in CDCl₃ of the eluted solution (flow conditions: residence time; 2 min, at 120 °C, 98% conversion, 15% yield) after drying with heating under reduced pressure. (b) ¹H NMR spectra in CDCl₃ of poly(cyclohexene oxide reported in [2].

References

- 1. Kaneda, K.; Haruna, S.; Imanaka, T.; Hamamoto, M.; Nishiyama, Y.; Ishii, Y. *Tetrahedron Lett.* **1992**, *33*, 6827–6830.
- 2. Yahiaoui, A.; Belbachir, M.; Soutif, J. C.; Fontaine, L. Mater. Lett. 2005, 59, 759–767.